

## **Determination Of The Optimal Parameters Of The Equipment To Obtain Fine Powders**

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### **Abstract.**

Currently, in terms of consumption of cement occupies a leading position among construction materials, but its production is expended a lot of energy, as in burying and grinding on materials at various stages. To reduce the power consumption can be under grinding clinker and additives in a closed cycle. However, given the large number of external factors to maximize the efficient use of a large number of co-operating complicated equipment is difficult task. To optimize the process of obtaining fine powders is proposed to obtain mathematical models derived from experimental results, taking into account the features included in the line of apparatuses. On the basis of these mathematical models is proposed to obtain the objective function to ensure optimum working conditions as all milling equipment, as well as individual elements included in its composition. The obtained

expressions allow also to obtain the production of powders with guaranteed technological properties.

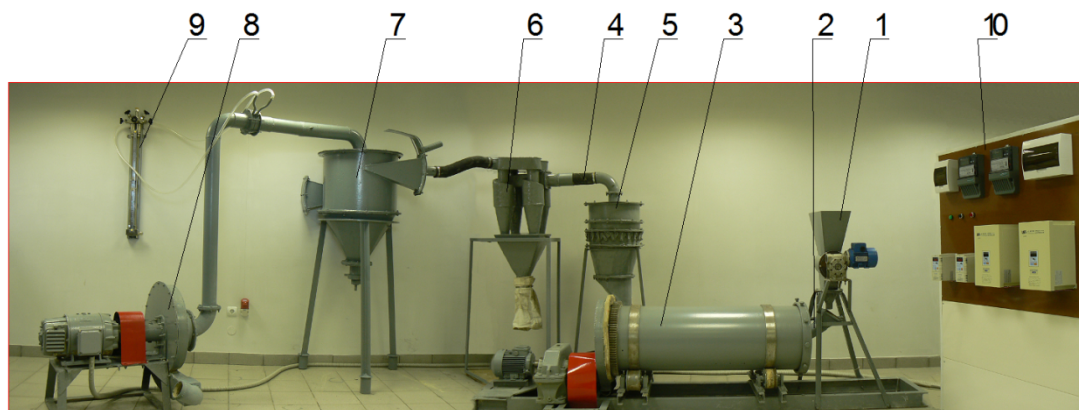
**Keywords:** fine powders, the regression equation, a closed circuit, an air separator, capacity, specific power consumption, efficiency.

### Introduction.

Preparation of fine powders with minimal cost in modern conditions of the industry is a very important task [1]. In most cases, this is possible only with the use of a closed circuit milling [2, 3, 4]. However, given the large number of external factors to maximize the efficient use of a large number of cooperating complicated equipment is a difficult task [5, 6]. The solution of such problems is possible in the preparation of mathematical models and find the optimum, in which there is maximum efficiency of the equipment operation. Given the complexity of the processes occurring in each of the apparatuses included in the process line of production of fine powder, analytical expressions describing the whole process become so cumbersome that they were being lost the original meaning of the event.

### Methods.

To study the process of grinding cement clinker and additives, we have developed an experimental installation closed circuit based on a ball mill shown in Figure 1.



**Figure 1.** Experimental installation closed circuit based on a ball mill: 1 – drum feeder; 2 – distributor; 3 – ball mill; 4 – the air; 5 – separator; 6 – cyclone; 7 – grain filter; 8 – blower; 9 – liquid differential pressure gauge; 10 – remote control

To optimize the process of obtaining fine powders it is convenient to build mathematical models derived from experimental results, taking into account the features included in the line of apparatuses. Given the large number of factors of the experiment to study the work of the grinding unit we selected as the main plan of the

experiment central composite rotatable plan full factorial experiment CCRP  $2^{5-1}$  FFE [7]. In accordance with the plan established five levels of factors: -1 – lower; 0 – average; +1 – top; -2, +2 – star.

All accepted factor levels are implemented on the model of a ball mill operating in continuous mode and correspond to the actual working conditions of ball mills closed circuit (Table 1). As the separation device used separator of air-flow centrifugal type.

**Table 1.** The investigated factors and varying levels CCRP  $2^{5-1}$  FFE

Factors	the code denoted	varying interval	$X = -2$ (star level)	$X = -1$ (lower level)	$X = 0$ (average level)	$X = +1$ (top level)	$X = +2$ (star level)
Circulating load, $c$ , %	$X_1$	50	50	100	150	200	250
Air velocity, $V$ , m/s	$X_2$	0.1	0.5	0.6	0.7	0.8	0.9
Partition position, $l_2/l_1$	$X_3$	0.25	0.50	0.75	1.00	1.25	1.50
Specific area partition $[\mu]$ , %	$X_4$	2	8	10	12	14	16
The frequency of rotation of the drum $[\psi]$ , %	$X_5$	0.07	0.62	0.69	0.76	0.83	0.90

To study the operation of the air separator chosen as the basic plan of the experiment central composite rotatable plan full factorial experiment CCRP  $2^3$  FFE (Table 2).

**Table 2.** The investigated factors and varying levels CCRP  $2^3$  FFE

Factors	Code denoted	varying interval	$X = -1.682$ (star level)	$X = -1$ (lower level)	$X = 0$ (average level)	$X = +1$ (top level)	$X = +1.682$ (star level)
Separating the airflow, $L$ , $m^3/h$	$X_6$	50	216	250	300	350	384
Rotor speed, $n$ , rpm	$X_7$	240	600	760	1000	1240	1400
The degree of overlap gate, $[\mu]$ , %	$X_8$	24	20	36	60	84	100

The mathematical model obtained as a result of treatment-experiment, are regression equations as a quadratic function:

$$P, Q, q, e, R = b_0 + \sum b_i x_i + \sum b_{ij} x_i x_j + \sum b_{ii} x_i^2, \quad (1)$$

where  $P$ ,  $Q$ ,  $q$ ,  $e$ ,  $R$ —parameters investigated in this case, accordingly, power consumption, capacity, specific energy consumption, efficiency of the air separation and the quality of the final product is determined in the control sieve residue, calculated during the experiment;  $b_0$ —free term of the equation;  $b_i$ ,  $b_{ij}$ ,  $b_{ii}$ —coefficients, accordingly, with linear parameters, when the effects of the interaction and quadratic terms;  $x_i$ ,  $x_j$ —varying levels of factors.

### The main part.

The resulting regression equation of the experiments allow to say the magnitude of the influence of different factors and their interaction effect on the value of the parameters  $P$ ,  $Q$ ,  $e$ ,  $R$  and their derivatives. But, given the large number of members of the regression equations, and impossible selection of the optimum possibilities simple enumeration values of factors we performed an experiment in the optimization of conditions for a minimum power consumption  $P$ ,  $Q$  high capacity ball mill closed circuit with guaranteed quality of the finished product defined by parameter  $R$ . The challenge is to find such a correlation factor, which would be observed at the maximum efficiency of the grinding process: minimum energy consumption with maximum performance. To find the optimum of the objective function, factor space, constituting a area of admissible values of the function, represented in the form of a hypercube with side equal to four units. To solve the problem of optimization of the grinding process in ball mill closed circuit is necessary to formulate a criterion of optimality, in other words — a qualitative assessment of the effectiveness of the process under various values of the adjustable parameters.

The optimality criterion can be adopted following objective function:

$$F(c, V, k, v, \psi, L, n, \mu) = a_1 \frac{P}{Q} + a_2 (R - R^*)^2 + a_3 f(c, V, k, v, \psi, L, n, \mu), \quad (2)$$

where  $a_1$ ,  $a_2$ ,  $a_3$ —weights regulatory significance (contribution) of a term, and taking into account the difference in the absolute values and the dimensions of the corresponding quantities;  $P$ —power consumed by the plant, calculated by the regression equation;  $Q$ —capacity milling unit, calculated according to the regression equation;  $R$ —quality of the final product, calculated by the regression equation;  $R^*$ —required quality of the finished product, and defined in the calculation;  $f$ —function of the input parameters, limiting the search for optimizing the values of the hypercube;  $c$ ,  $V$ ,  $k$ ,  $v$ ,  $\psi$ ,  $L$ ,  $n$ ,  $\mu$  — circulating load, the air velocity in the drum of the mill, the ratio of the lengths of mill chambers, the living section partitions, frequency of rotation of the mill drum, the flow separation air, velocity of the rotor in the air separator, aerodynamic parameter.

Optimization of the grinding process carried out by minimizing the function  $F(c, V, k, v, \psi, L, n, \mu)$  by the method of fastest descent [8, 9, 10]. By choosing the values of the coefficients  $a_1$ ,  $a_2$ ,  $a_3$  considered several kinds of functions  $F$ —optimality criteria with qualitative differences. Before proceeding to discuss the results of the calculations necessary to make the following notice. Since the experimental installation,

as in some sense the grinding unit geometrically similar industrial installations, and dynamic similarity does not, we were interested in not the absolute values of the input factors and tendencies of their changes when you change the requirements for the results of the process parameters of grinding. With that said type of function has been selected and arranged numerical calculations. The results of the first series of calculations are shown in the figure. The calculations were performed with  $a_1=0$ ,  $a_2=10$ ,  $a_3=0$  for different values of  $R$ . Thus, we studied the effect on the values of input factors increase or decrease the fineness of the finished product.

As seen in Figure 2a, to obtain a product with small residues on the sieve 008 must provide a minimal circulating in the system load; velocity of the air in the drum mill, shift towards lower values of the parameter  $V$ ; minimum length of fine grinding chamber corresponding to the adopted plan of the experiment; minimum carrying capacity in inclined mill partition of the parameter  $[\nu]$ , the design to the second, and vice versa, and the minimum frequency of rotation of the drum mill  $[\psi]$ . This provides a long time in the drum of the mill and, therefore, higher degree of comminution.

Figure 2b shows the technological characteristics of the process of grinding in ball mills closed circuit for the corresponding values of input factors. These values are input factors are explained as follows: to provide greater fineness in the drum mill should be the minimum amount of material to be ground, which is provided with a minimum circulation load. The air velocity in the mill drum should thus not provide intensive removal of material from the grinding mill drum, thus increasing time in the drum mill.

Increasing the length of the second chamber allows you to increase the fine grinding fineness at the expense of long term exposure small ball load on sample material and transport capacity reduction due to partition  $[\nu]$  possible movement material from the first chamber to the second and back, crank mill drum to  $360^\circ$  also increases the time material in the mill and, therefore, leads to increased fineness of the grinded material.

Minimum residues of grinding material on the control sieve are obtained at lower drum mill velocity  $[\psi]$ , due to the predominance of the abrasive effects of grinding media on the ground material.

For example, to obtain a product with a 5 %  $R$  with a minimum consumption of electric power needed to circulating load equal to 50 %; air velocity  $V$  in the drum mill – 0.56 mps; the ratio of the lengths of the chambers  $(l_2/l_1) = 1.4$ ; living section of the partition  $[\nu] = 15\%$ , and the relative velocity of the drum mill  $[\psi] = 0.665$ . With the increase in circulating load we can see increase in the parameter  $R$ . The growth parameter with the same parameters  $V$  causes coarsening of the material by increasing the average size of the carrying off the drum mill grinding material particles. Analysis of expressions suggests that the coarsening of the material should be reduced the chamber of fine grinding and increase the relative velocity of the drum mill. Firstly, this is due to the fact that increases the mass fraction of the crushed material in the drum mill (increases circulation load) that is needed for a greater share of the impact of the grinding media and ensured that bigger length of the first chamber and, secondly, the

greater frequency of rotation of the drum mill that increases accordingly, the impact forces.

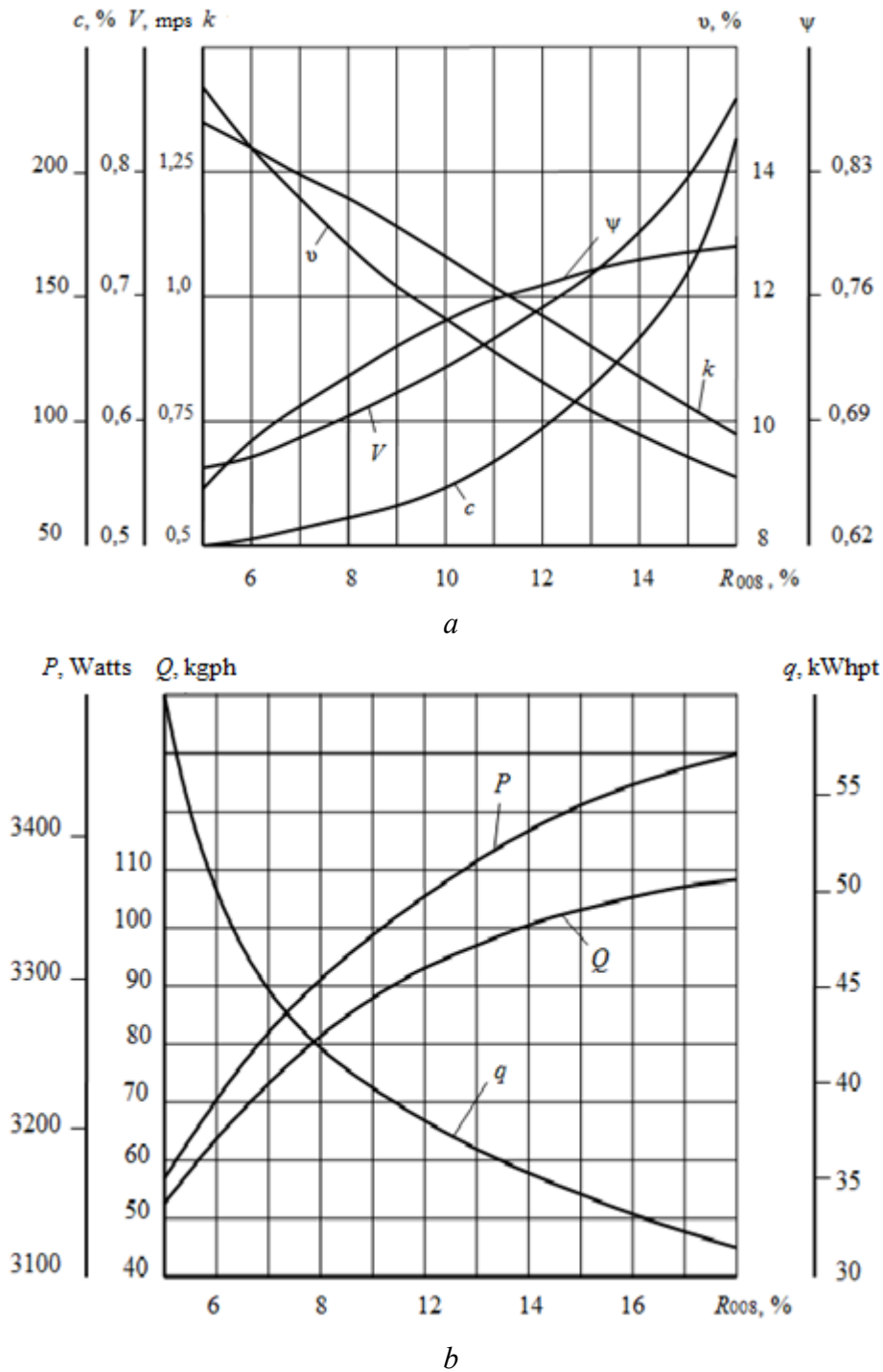


Figure 2. Dependence of the optimization of input factors (a) and the values of the process parameters ball mill closed circuit (b) of the fineness of the finished product at minimization of specific energy consumption

Substituting the resulting solution of the objective function values of the varied factors in its minimization ( $x_1, x_2, x_3, x_4, x_5, x_6, x_7, x_8$ ) in the corresponding regression equations define consumed power setting  $P$ , its capacity is of appropriate quality of the final product  $Q$ , and specific energy consumption  $q$  on grinding while maintaining the defined quality indicators grinding system (see Figure 2b).

Increasing the capacity of the plant is accompanied by increasing levels of consumption and its power. The maximum contribution to the increase in the parameter  $P$  exert in increasing the frequency of rotation of the drum mill and the velocity of the air in the drum mill and, to a lesser extent – the growth of circulating load. The remaining two parameters –  $k$  and  $[\nu]$  a significant impact on the value of  $P$  does not have, as it does not alter the character of the movement of the grinding load during grinding material. With the coarsening of the material from 5 to 16% increase power consumption is 9.5%, i.e. from 3154 to 3456 Watts. In order to optimize the closed circuit ball mill to obtain the minimum power consumption in the formula (1) take the following values of weighting coefficients  $a_1 = 10, a_2 = 0, a_3 = 0$ .

Calculations based on the above given method showed that the minimal power consumption is observed at  $c = 208\%$ ;  $V = 0.87 \text{ mps}$ ;  $k = 1.45$ ;  $[\nu] = 8\%$  and  $[\psi] = 0.85$  and is 24.28 kWhpt. At the same plant capacity is 100.4 kgph and consumption of energy – 2437 Watts.

Maximum capacity ball mill is 111.36 tph for the following values of the varied factors:  $c = 110\%$ ;  $V = 0.9 \text{ mps}$ ;  $k = 0.78$ ;  $[\nu] = 8\%$ , and  $[\psi] = 0.75$ . The power consumed by the installation, in this case is 3125 Watts, with specific power consumption  $q$ , equal to 28.06 kWhpt.

With optimization of only an air separator (ball mill was turned off and the power of the air separator is carried autonomously) with specific surface of powder equal to  $3500 \text{ cm}^2/\text{g}$  maximum capacity  $Q$  air separator is observed for the following values of variable parameters: airflow separation  $L$  is  $375.4 \text{ m}^3/\text{ph}$ ; separator rotor velocity is  $732.2 \text{ rpm}$ ; aerodynamic separator parameter  $[\mu]$  93.14% and  $Q$  is 366.5 kgph.

The separation efficiency of an air separator for these values is 74.5%.

The maximum separation efficiency  $E$  air separator is observed for the following values of variable parameters: airflow separation  $L$  is  $355.1 \text{ m}^3/\text{ph}$ ; rotational velocity of the rotor is  $1348.3 \text{ rpm}$ ; aerodynamic parameter separator  $[\mu]$  is 79.68% and  $E$  86.33% is. The capacity of a separator at these values constitutes 302.56 kgph at a specific surface of the finished product  $4200 \text{ cm}^2/\text{g}$ .

## Conclusions.

In the course of the research were obtained regression equations work grinding unit closed circuit ball mill and an air separator and the proposed objective function, which allows to determine the optimal operating conditions of both the grinding unit as a whole and its individual elements. The values of the factor levels at which a minimum energy consumption of the entire grinding unit, its maximum capacity, the maximum capacity of an air separator and its maximum efficiency.

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