

Assessment of Losses of Reheating Furnace in a Steel Re-Rolling Mill

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Abstract

Thermal efficiency of process heating equipment, such as furnaces, ovens, heaters, and kilns is the ratio of heat delivered to a material and heat supplied to the heating equipment. The purpose of a heating process is to introduce a certain amount of thermal energy into a product, raising it to a certain temperature to prepare it for additional processing or change its properties. To carry this out, the product is heated in a furnace. This results in energy losses in different areas. For most heating equipment, a large amount of the heat supplied is wasted in the form of exhaust gases.

Keywords: Steel plant, Energy Efficiency, Furnace, Reheating Furnace, losses, SRRM.

INTRODUCTION

Reheating Furnace is an equipment to heat materials for change of shape (rolling, forging etc.) or change of properties (heat treatment). Furnaces must be designed and operated to achieve:

- A desired production rate
- Acceptable product quality (e.g. temperature uniformity in steel slabs, time at temperature in brick kilns)
- Maximum thermal efficiency
- Pollution emissions (e.g. NO_x) within acceptable or legal limits.

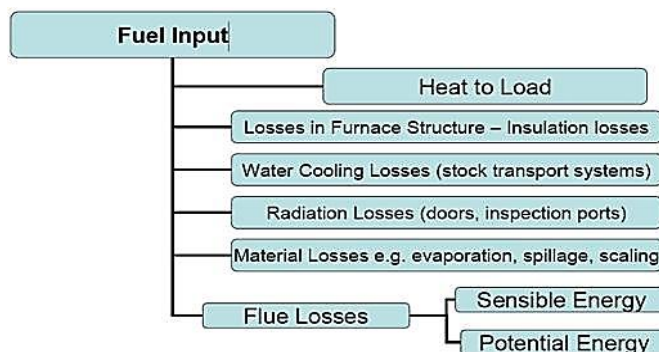


Figure 1:- Losses in furnaces

Because of their high temperature, furnaces are large users of fossil-fuel energy. The above simple diagram lists the main losses on a typical furnace. Flue gases are usually main source of wasted energy.

The present study evaluates the losses evaluation of reheating operation of steel in the reheating furnace at XYZ steel plant.

LOSSES IN FURNACE

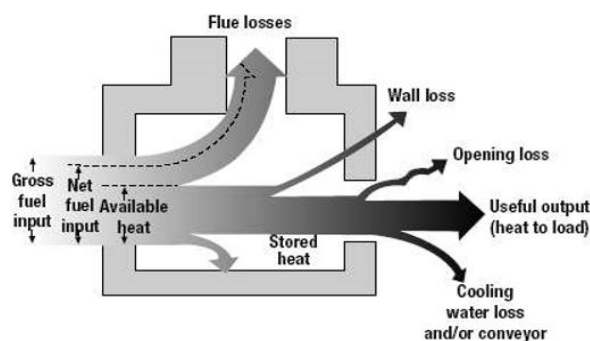


Figure 2:- losses diagram of a furnace

A. Flue Gas Losses:

Flue gases represent the main energy loss on furnaces because of their high temperature [1]. Sensible losses as a percentage of net heat input can be estimated from the following graph for different percentage levels of excess air.

B. Wall losses

Wall or transmission losses are caused by the conduction of heat through the walls, roof, and floor of the heating device [2].

C. Cooling Media Losses

Cooling protects rolls, bearings, and doors in hot furnace environments, but at the cost of lost energy. These components and their cooling media (water, air, etc.) become the conduit for additional heat losses from the furnace [3].

D. Air infiltration

Excess air does not necessarily enter the furnace as part of the combustion air supply. It can also infiltrate from the surrounding room if there is a negative pressure in the furnace. Because of the draft effect of hot furnace stacks, negative pressures are common, and cold air slips past leaky door seals and other openings in the furnace.

E. Radiation (opening) losses

Furnaces and ovens operating at temperatures above 1,000°F might have significant radiation losses. Hot surfaces radiate energy to nearby colder surfaces, and the rate of heat transfer increases with the fourth power of the surfaces absolute temperature [4].

F. Water losses

Water flow rate, temperature difference between water in and out, etc.

G. Wall, hearth and roof losses

Outside area of furnace, thickness and thermal properties of refractory and insulation, surface

Temperature, etc.

H. Atmospheric losses

Temperature difference between in and out

Atmosphere and atmosphere flow rate.

Table 1:-Furnaces installed in the Plant

| Location /Furnace | Nos |
|-------------------|-----|
| Stackle Mill | 2 |
| Strip mill | 1 |
| Annealing furnace | 1 |
| Finishing furnace | 1 |
| Boggie furnaces | 1 |

To evaluate the losses of reheating operation of steel in the reheating furnace at XYZ steel plant, we have restricted our study to Stackle mill only.

Stackle mill has 2 furnace, walking beam & Preheating Furnace. Fuel used for furnace is LPG & LVFO/HSD, depending upon the different grades. Detailed description of fuel, raw material specifications & Recuperator are as follows:-

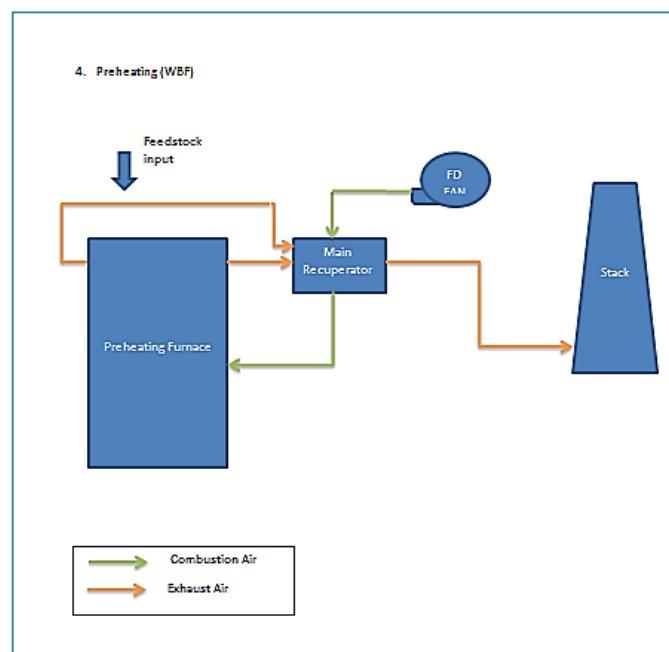


Figure 3: Block diagram of preheating furnace

CASE STUDY

There are total 8 furnaces installed in the plant XYZ. Out of these eight, 2 are electric arc furnace while rests are fuel fired. Furnaces installed in the plant are[5]:-

Specifications

Table 2: description of furnaces of Stackle mill

| S.No | Description | Unit | Flat | JBS |
|------|-----------------------------------|-----------|----------------|----------------|
| 1 | Type of Fuel Used in Furnace | | FO | LVFO / HSD |
| 2 | <i>Cycle Time</i> | | | |
| | Productivity | MT/Hr | 45 | 12 |
| | Coil to Coil Gap | Min | 2 | 6 |
| 3 | <i>Raw Material Specification</i> | | | |
| | Bloom Size (T X W X L) | mm | 200X200X5050 | 200X260X3350 |
| | Bloom Weight | MT | 1.53 | 1.33 |
| | Bloom Size (T X W X L) | mm | 200X260X5050 | |
| | Bloom Weight | MT | 2.00 | |
| 4 | <i>Recuperator Data</i> | | | |
| | Inlet | °C | 550-630 | 630-700 |
| | Outlet | °C | 180-210 | 200-220 |
| | Hot Air | °C | 280-350 | 330-400 |

Furnace operating parameters are as follows:-

Table 3: furnace-operating parameters of Stackle mill

| Furnace Operating parameters | | | | | | |
|------------------------------|----------------------|-----------|-----------|-----------|-----------|----------------|
| Grade | Zone Wise Temp (° C) | | | | | Holding (Hrs.) |
| | THZ A | THZ B | BHZ | TSZ A | TSZ B | |
| Flat | 1190-1220 | 1190-1220 | 1080-1110 | 1200-1220 | 1200-1220 | 3 to 5 |
| JBS | 1250-1270 | 1260-1280 | 1235-1255 | 1250-1270 | 1260-1280 | 8 to 9:30 |

Table 4: Blower details of Stackle mill

| | PHF | | WBF | |
|----------------------------------|--------------|-----------|-------------|-----------|
| | Comb. Blower | Atomiz. | Comb Blower | Atomiz. |
| No Of Blower Installed | 2 | Comp. air | 3 | Comp. air |
| No Of Blower Running at one time | 1 | | 2 | |
| Flow (NM3/Hr) | 29000 | | 9.86 m3/sec | |
| Flow in M3/Sec | 7.3 | | 9.86 | |
| Flow in NM3/Hrs. | 29000 | | 39166 | |
| Pressure (mmwc) | 900 | | 1000 | |
| Motor | 132 kW | | 132 kW | |
| RPM | 1470 | | 1480 | |

Calculations for Re-heating Furnace

In order to calculate the performance of the preheating furnace we take in to consideration the following [6][7]

Furnace Specifications

Table 4: Specifications for preheating furnace

| Sr. No | Parameter | Units | Value |
|--------|-------------------------------|-------|--------|
| 1 | Capacity | TPH | 150 |
| 2 | Dimensions: | | |
| | Length | m | 15.5 |
| | Width | m | 11.9 |
| | Height | m | 2.5 |
| 3 | Steel Grade | | JT1250 |
| 4 | Fuel Used | | LDO |
| 5 | Feed-in Temperature | °C | 70 |
| 6 | Feed-out Temperature | °C | 500 |
| 7 | Ambient Air Temperature | °C | 38 |
| 8 | Hot air Inlet Temperature | °C | 273 |
| 9 | Recuperator Inlet Temperature | °C | 497 |
| 10 | Flue gas outlet Temperature | °C | 340 |

Fuel Consumption

Fuel consumption of the Furnace was 727 kg/Hr.

Table 5: Fuel Consumption

| Fuel Reading | | |
|--------------|---------|---------------|
| Fuel | Units | Meter Reading |
| LDO | Kg / hr | 727 |

Surface Temperatures

Temperatures had been measured using IR & Thermal Imager.

Table 6: Measured Surface Temperature

| Sr. No | Surface temp | Units | Mini mum | maxi mum | Avg. |
|--------|--------------|----------|----------|----------|------|
| 1 | Right wall | degree C | 75 | 146 | 105 |
| 2 | Left wall | degree C | 50 | 113 | 92 |
| 3 | Roof | degree C | 58 | 70 | 66 |
| 4 | Front wall | degree C | 53 | 162 | 70 |
| 5 | Back Wall | degree C | 152 | 263 | 202 |

Efficiency of Furnace

Calculated Efficiency using various formulas [8] of the furnace was 27 %.

Table 7: Efficiency of furnace

| Parameter | Units | Value |
|-------------------------------------|----------|------------|
| Actual Fuel Consumption (Measured) | kg/Hr | 727 |
| Cycle time of furnace | Hr | 2 |
| C.V. of Fuel(L.D.O.) | kCal/kg | 10600 |
| Initial Temperature of Bloom | °K | 343 |
| Final Temperature of Bloom | °K | 773 |
| Temperature Difference | °K | 430 |
| Cp of Bloom | kJ/kg.K | 0.45 |
| Slab quantity in furnace | Nos. | 8 |
| Net Weight of Feed stock in furnace | kg | 89759 |
| Heat output (Q) | kCal | 4155112 |
| Fuel consumption for cycle | kg | 1454 |
| heat input | kCal | 15412400 |
| Efficiency | % | 27% |

Radiation Losses calculation

The radiation loss can be calculated by knowing how much of heat is lost in the form of radiation [9]

Table 8: Radiation losses of Furnace

| Parameter | Units | Value |
|--|------------------------|--------|
| <i>Ambient temperature</i> | °K | 313 |
| <i>Total Surface Area of the furnace</i> | | |
| Right wall | m ² | 38.75 |
| Left wall | m ² | 38.75 |
| Ceiling | m ² | 184.45 |
| Front wall | m ² | 29.75 |
| Back wall | m ² | 29.75 |
| <i>Average wall temperature</i> | | |
| Right wall | °K | 378 |
| Left wall | °K | 365 |
| Ceiling | °K | 339 |
| Front wall | °K | 343 |
| Back wall | °K | 475 |
| Emissivity of external wall surface | E | 0.75 |
| <i>Right wall</i> | | |
| Losses through right wall | kCal/hr/m ² | 802 |
| Overall heat losses through the right wall | kCal/hr | 31076 |
| <i>Left wall</i> | | |
| Losses through left wall | kCal/hr/m ² | 606 |
| Overall heat losses through the left wall | kCal/hr | 23464 |
| <i>Ceiling</i> | | |
| Losses through Ceiling | kCal/hr | 296 |
| overall Losses through Ceiling | kCal/hr | 54685 |
| <i>Front wall</i> | | |
| Losses through front wall | kCal/hr/m ² | 310 |
| Overall heat losses through front wall | kCal/hr | 9216 |
| <i>Back wall</i> | | |
| Losses through back wall | kCal/hr | 2783 |

| | | |
|-------------------------------------|----------|-------------|
| overall Losses through back wall | kCal/hr | 82806 |
| Overall heat losses through surface | kCal/hr | 201247 |
| Energy input to furnace | kCal/hr | 7706200 |
| losses through radiation | % | 2.6% |

Thus, the radiation losses of the furnace was calculated as 2.6% only.

Flue gas losses

In most cases these account for the majority of the losses in the furnace [10] and it can be see below in our case too

Table 10: Radiation losses of Furnace

| Parameter | Units | Value |
|------------------------------------|------------|-----------|
| FG Temp | °K | 833 |
| Allowable stack Temp | °K | 473 |
| flow rate | kg/hr. | 1526 |
| Specific Heat | kJ/kg.K | 1.17 |
| Waste Heat Potential | kCal/hr | 2691199 |
| operational hours | hr. | 24 |
| operational Days | days | 320 |
| Annual waste heat saving potential | MCal/Annum | 8267364 |
| Flue gas Losses | % | 35 |

Flue gas losses was 35%, which was highest of all losses hence proving to be the area of major losses.

DISCUSSION

This assessment of energy found the following areas of efficiency improvement [11].

A. Waste heat recovery

The flue gases coming out from the reheating furnace contain substantive amount of heat energy, which can be reused.

B. Load Preheating

The billets are loaded in the furnace at ambient temperature, so heat is required for initial heating of that billets. The sensible heat going out of the stack along with flue gases can fulfill this heat requirement.

C. Preheating Combustion Air

Combustion air can be preheated in the recuperators by using heat from waste gases from the furnace. This reduces fuel consumption thus reducing the environmental impacts [12] and it also increases flame temperature and improves furnace efficiency.

D. Proper maintenance of the furnace

As observed at XYZ Plant there is lack of maintenance inside the furnace. At the shutdown period there are too many cracks and erosions observed on the refractory lining made by 60% alumina brick (fire clay bricks) at the inside wall of the furnace. To overcome losses due to the lack of maintenance the 90% high alumina castable can be used to fill the cracks so that heat transfer must be resisted from inside to the outside wall of the furnace.

E. Proper utilization of Control system

In the reheating process, furnace pressure and temperature control have significant effects on energy efficiency improvement. The negative pressure inside a reheat furnace can cause ambient air to enter into the reheat furnace, which needs extra energy to heat the leakage air to flue gas temperature. Furnace pressure controller can keep a positive pressure in the furnace chamber to reduce atmosphere losses.

CONCLUSION

The energy efficiency reported was 27 %. The flue gases loss is reported to be 35 %, which is the largest among all accounted losses during the operation.

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